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# Highlights

- In electrocatalysis, complex nonlinear and non-monotonic coupling arises in the boundary region between metal and electrolyte
- A recent theoretical framework demonstrates how to handle this coupling
- Approaches in first-principles electrochemical modeling need to be modified to consistently treat nonlinear and non-monotonic charging effects

# Approaching the Self-Consistency Challenge of Electrocatalysis with Theory and Computation

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#### Abstract

This opinion piece centers around challenges involved in developing first-principles electrochemical methods. In recent years, theory and computation have become quintessential tools to navigate the parameter space that controls the activity and stability of electrocatalytic materials and electrochemical devices. Viable methods process as input details on materials structure, composition and reaction conditions. Their output includes metrics for stability and activity, phase diagrams, as well as mechanistic insights on reaction mechanisms and pathways. The core challenge, connecting input to output, is a self-consistency problem that couples the electrode potential to variables for the electronic structure of the solid electrode, solvent properties and ion distributions in the electrolyte as well as specific properties of a boundary region in between. We will discuss a theoretical framework and computational approaches that strive to accomplish this feat.

Keywords: theoretical electrocatalysis, electric double layer, metal charging relation, continuum solvation models, first-principles electrochemistry, electronic density functional theory

## 1. Introduction

Electrocatalysis is becoming for electrochemical energy technology what semiconductor physics has long been for computer technology: the fundamental discipline to bring forth advances in cost reduction, power performance, durability and lifetime, while submitting to requirements in terms of

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safety and materials abundance [1, 2]. Contributions and impact in the field of electrocatalysis exhibit exponential growth, with efforts headed towards new materials and fabrication approaches for next generation electrochemical systems in energy harvesting, water treatment, production of fuels and chemicals, materials processing and biosensing.

In addition to maintaining a justified focus on precious metal-based electrocatalysts such as Pt and Pt-based alloys [3, 4, 5], escalating efforts strive to harness unusual and opaque properties of transition metal oxides [6, 7], nitrides [8, 9], phosphides [10, 11, 12, 13, 14], and chalcogenides [15, 16, 17], as well as 2D electronic materials [18, 19] and macromolecular precious metal-free electrocataysts [20, 21].

Finding the best materials for emerging energy, water or sensor technologies demands scientific strategies that (i) utilize materials selection criteria based on a small set of performance and stability descriptors [3, 22, 23], (ii) employ efficient tools to navigate a complex parameter space, and (iii) implement smart approaches in electrode design and fabrication based on knowledge of reaction mechanisms, pathways and conditions.

Materials fabrication and characterization increasingly look out to theory and computation for guidance. Theoretical and computational electrocatalysis strives to relate atomic structure, composition, and electronic structure of electrocatalytic materials to measurable performance and stability descriptors, as illustrated in Figure 1. However, to become more than tools for materials screening and comparative analyses, theory and computation must be physically consistent and accurate; utilize a reasonably complex (adaptive) representation of the real electrochemical interface with a minimal set of assumptions; and provide fundamental mechanistic insight and predictive capabilities.

The electrified electrochemical interface as the archetypal electrochemical system is usually a substructure of a porous composite electrode in an electrochemical device, where the interplay of transport and reaction determines distributions of reaction conditions and rates. Well-established models describe the operation of such electrodes [24]. Focusing on theory and modeling of the interface itself, the main challenges are to understand how the nature and structure of electrode material, electrolyte and boundary region in-between impact the energetics and dynamics of adsorption and charge transfer processes; how impurities or adsorbed intermediates affect pathways of multistep reactions and reactivity [25]; and how solvent species and ions modulate interfacial properties and reaction conditions [26].

Theoretical electrocatalysis is closely interwoven with the quintessential theories of electrified interfaces [27] and charge transfer [28, 29, 30] and it draws upon inventories of condensed matter physics, surface science, heterogeneous catalysis, and chemical kinetics. Modern developments in this multidisciplinary field circulate under the label first-principles electrochemistry (FPEC) [31, 32] or alike [33].

Computational approaches finding a growing community of users include the so-called *computational hydrogen electrode* (CHE) based on standard-type electronic DFT, the *generalized CHE* (GCHE) that employs nonequilibrium Green's functions and electronic DFT (NEGF+DFT) [34], or implementations that combine electronic DFT for the electrode region with continuum mean field theories or classical DFT for the electrolyte region, like JDFTx [35] or VASPsol [36].

"[Figure 1 should be placed here. The basic program for theoretical electrocatalysis.]"

# 2. Challenges and approaches

Figure 2 epitomizes the litmus test and potential pitfall for approaches in theoretical and computational electrocatalysis. Extracted from a paper published in the mid 1970s by Frumkin and Petrii [37], it shows surface excesses of sodium cations and sulfonate anions near a Pt electrode as a function of the metal phase potential,  $\phi^{\rm M}$ . It thus portrays, more or less explicitly, the metal charging relation,  $\sigma^{\rm M} = f(\phi^{\rm M})$ , as "seen" by free ions in solution. This nonlinear and non-monotonic charging relation demonstrates that in general the effective metal surface charge, and all dependent properties, cannot be deduced by linear extrapolation from the potential of zero charge with the double layer capacitance as a proportionality constant.

Recent experiments [38, 39, 40] attributed the observations in Figure 2 to charge polarization effects caused by formation of a (sub-)monolayer oxygen adatoms at the surface. Existing FPEC approaches fail to reproduce this charging relation since they have a linear extrapolation of  $\sigma^{\rm M}$  as function of  $\phi^{\rm M}$  built into them or miss certain aspects of the nonlinear coupling of components and properties that define the interfacial region.

"[Figure 2 should be placed here. Frumkin.]"

Figure 3 illustrates schematically the typical modeling domain and the fundamental theoretical challenge. The Galvani potential,  $\phi^{M}$ , in the bulk of the metal phase (at point A) is specified relative to a reference Galvani

potential in the bulk electrolyte phase (at point B),  $\phi^{S}$ , with A and B located far away from the interfacial region. The solution phase potential thus establishes a reference for the potential scale, which can be fixed as  $\phi^{S} = 0$ , without having to invoke a thermodynamic construction that is strictly valid only at a certain equilibrium condition of the interfacial system, as is the case for the CHE. Complete solution of the interface problem must fulfill two essential conditions: (1) it must generate a continuous potential profile between A and B; (2) it must account self-consistently for the coupling of relevant variables that define the properties of different interface regions en route from A to B.

Figure 3 resolves the different components of the interfacial system, including electrode material, chemisorbed surface species, a structured region of interfacial solvent molecules, and a diffuse electrolyte region extending towards the bulk. The coupled variables in the system include the electrochemical potential of electrons in the electrode, the electrode surface state represented by the surface atom configuration and chemisorbed species, an order parameter for the preferential orientation of interfacial solvent molecules, solvent dielectric or polarization properties, and the ion density in the electrolyte. The main function to solve for is the electrostatic potential profile along the path from A to B, as a function of  $\phi^{\rm M}$  and pH (and ion concentrations) in the bulk electrolyte.

For the electrode region, Kohn-Sham DFT (KS-DFT) at the level of the generalized gradient approximation (GGA) is used to calculate ground state electronic densities, energy contributions and forces [41]. Systems with onsite Coulomb interaction of strongly localized electrons (typically, d- or f-electrons) require addition of a Hubbard-like interaction term [42]. Interaction parameters for this DFT+U approach [43] are obtained from linear response theory [44]. This correction is required for calculating the properties of transition metal oxides [45]. Needs and challenges involved in extending DFT approaches towards treatment of electron dispersion interactions were discussed in Ref. [46]. The accuracy of various dispersion-corrected DFT functionals was assessed in Ref. [47, 48] for the Pt-water system.

The electrolyte region, consisting of solvent molecules and ions, determines the system's capacity to store charge at the electrochemical interface. The size of the electrolyte region relevant for electrochemical studies depends on the Debye length. This length could lie in the range of 10 nm or more, rendering a quantum mechanical treatment infeasible. Theoretical approaches to describe this region must deal with solvent polarization,

steric effects and Coulomb interactions. Due to reactive events and thermal effects, the electrolyte region reorganizes dynamically. Thermodynamic sampling of electrolyte configurations is thus needed for the calculation of thermodynamic averages. This statistical sampling can be done using continuum solvation models (CSM), surveyed in Refs. [49, 50], in conjunction with mean field approaches like Poisson-Boltzmann (PB) or modified Poisson-Boltzmann (MPB) theory [51, 52, 53]. An alternative to continuum theories is the rigorous classical density functional theory of liquids [54]; it calculates thermodynamic functions by variational free energy minimization, rendering it computationally more efficient than molecular dynamics simulations. As for the latter, there are currently no reports on explicit simulations of electrochemical interfaces based on QM/MM, as are widely popular in other fields [55].

Combination of electronic structure calculations for the electrode region with different treatment of the solvent region results in three main classes of FPEC approaches, which are (i) the computational hydrogen electrode (CHE) of Nørskov, Rossmeisl and others [56, 57, 58], (ii) a standard approach (DFT-CSM/MPB) that combines electronic DFT with mean field theories for the electrolyte region, pioneered by Otani and Sugino [59] and developed further by Jinnouchi and Anderson [49] as well as Dabo, Bonnet and Marzari [60], and (iii) joint density functional theory (JDFT) that combines electronic and classical DFT for the respective regions [35, 61].

All of these approaches and their numerous derivatives (too many to cite) are heavily preoccupied with two crucial questions: how to fix a potential scale and how to maintain electroneutrality in the system? As for the first point, in principle, this must be done by adding or deleting a sufficient number of electrons to the system - meaning that electrons are treated grand-canonically, as proposed originally by Lozovoi et al. [62] - to tune the electrochemical potential of electrons to a desired value [63]. Next, in order to maintain electroneutrality countercharge must be added. This has been done in different ways. In the CHE protons and electrons are added pairwise; this incurs a problem of an unphysical discreteness of charge amounts that could be addressed by increasing and extrapolating cell size. Lozovoi and Alavi employed a Gaussian charge sheet to add counter charge [64], whereas Taylor et al. added a uniform charge background [65].

These ad hoc approaches to the charging problem encountered the difficulty of adjusting to the correct value of the electric field at the interface. Otani and Sugino [59] tried to overcome this problem by combining KS-DFT

with MPB theory to calculate distributions of ion density and electric field in the interfacial region. Jinnouchi and Anderson [49] as well as Dabo *et al.* [60] refined this approach by connecting DFT and MPB approaches through a smooth dielectric continuum model for the solvent polarization that had been developed by Fattebert and Gygi [66]. The JDFT approach calculates the ion distribution self-consistently [61].

Having deposited a certain number of extra electrons on the metal surface and balanced it out with ionic charges on the solvent side, another problem arises: properties of the boundary region will respond to the electrode charging conditions, and this response could be highly nonlinear, invalidating simple potential extrapolation schemes and not accounted for in approaches discussed to this point. A shift in  $\phi^{\rm M}$  and  $\sigma^{\rm M}$ , will induce changes in the chemical surface configuration. These may involve modification of surface electronic states, short range electronic interactions with near surface species, bond formation (chemisorption), or orientational ordering of polar solvent molecules. For instance, in the case of a Pt electrode, a shift to high  $\phi^{\rm M}$  induces oxygen chemisorption and oxide layer growth [67, 68, 69]. For Ni oxyhydroxide under alkaline conditions, deprotonation of the surface occurs [70]. Such changes disturb the interfacial electric field, as seen in pronounced work function shifts [71], which cannot be handled by any of the FPEC approaches developed to date.

Potential-dependent surface configurations, e.g., involving chemisorbed species formed during reactive events, must be accounted for, necessitating in principle dynamic (or reactive) simulation approaches. Moreover, correct treatment of the properties of interfacial solvent molecules demands extensive thermodynamic sampling of configurations of near-surface solvent layers using ab initio MD [71, 72]. It turns out that the boundary region is indeed the most complex part of the electrochemical interface and its description is highly specific for particular electrode material, electrolyte composition, environmental conditions and potential regime. Next, we will briefly review a theoretical framework that illustrates the intricacies introduced by this region, to provide a proper basis for discussing current limitations and future needs to be addressed by next-generation FPEC approaches.

"[Figure 3 should be placed here. Interface.]"

#### 3. Theoretical framework

A theoretical approach to solve the interface problem, depicted in Figure 3, was developed in Ref.[73] and refined in Ref.[74]. This mean field approach focuses on interfacial charging effects and it was developed for the Ptelectrolyte interface. It considers the metal as an interface with an effective potential-dependent  $\sigma^{\rm M}$  and covered by a (sub-)monolayer of chemisorbed oxygen, which is treated with a thermodynamic submodel. A water layer submodel accounts for ordering of water dipoles relative to the surface with an Ising-like two-state approach. PB or MPB theory [51, 52, 53] are used to solve for ion and potential distributions in the electrolyte. The submodels for the different system components are self-consistently coupled resulting in two equations for the variables  $\sigma^{\rm M}$  and X, where X is the dimensionless adsorption energy of interfacial water molecules.

For the Pt-electrolyte system, the oxide layer submodel is the crucial link that connects metal and electrolyte regions. The experimental relation between oxide species coverage and  $\phi^{\rm M}$  is used to pin the potential scale to an experimentally accessible scale, such as the SHE scale. For other potential ranges and other materials, different experimental relations for the interfacial configuration must be used to pin the potential scale, e.g., the degree of surface deprotonation of Ni oxyhydroxide. Parameters that define the dipolar field generated by the layer of chemisorbed oxygen are calculated with KS-DFT

The fully parameterized model reproduces the non-monotonic charging relation as shown in Figure 2 and predicts a negative capacitance in the high potential region [78]. Moreover, it predicts the impact of pH on the metal charging behaviour [73]. It was applied to rationalize electrochemical processes in a water-filled nanopore with Pt plated walls [75], the particle proximity effect in nanoparticle electrocatalysis [76], and induced charge effects by an ionomer skin layer in catalyst layers of PEM fuel cells [77]. In combination with microkinetic modeling and input of basic boundary layer and reaction parameters from electronic DFT, the model allowed the oxygen reduction reaction to be deciphered and effective electrode parameters to be calculated [78], as explained in Figure 4. The utility of this approach remains to be demonstrated for other materials and conditions.

"[Figure 4 should be placed here. Coupling scheme of theory.]"

# 4. First-principles electrochemistry: status and path ahead

How well do current FPEC approaches address the fundamental challenge of electrocatalysis, depicted in Figure 1? What contributions to understanding basic electrocatalytic phenomena, deciphering reaction mechanisms, and developing advanced materials can they make? What methodical improvements will be needed in the future?

The CHE has been the most versatile and successful computational approach to date. It relates the potential scale to a thermodynamic reference and postulates a linear free energy relationship for the electrochemical potential (LFER-EP) of electrons. The CHE enforces a strict coupling of electron and proton transfer [80]. It gets by without explicitly treating solvent and electrolyte phenomena, then again implying that it blinds out the impact of electrode potential on bond strengths, adsorbate formation, and solvent polarization in the boundary layer. Generalizations using thermodynamic extrapolation schemes [81] or *ab initio* molecular dynamics for the near-surface solvent region [82] strive to address these shortcomings.

The CHE has proven useful in comparative evaluation of mechanisms and pathways of electrocatalytic reactions in fuel cells, batteries, electrolyzers, fuel production and CO<sub>2</sub> reduction. It demonstrated sufficiency of a single descriptor approach, rooted in scaling laws [84], to screen transition metal alloys for electrocatalytic activity [83] and enabled calculation of surface Pourbaix diagrams [85]. These outcomes are largely owed to the capabilities of KS-DFT to accurately reproduce electronic properties of metals.

The CHE approach does not pretend to mimic structure and properties of real electrochemical interfaces. Strictly speaking it is not an FPEC approach. In principle, FPEC approaches like DFT-CM/MPB or JDFT should provide equal capabilities as the CHE in comparative materials evaluation, analyses of reaction mechanisms and pathways, and determination of phase equilibria, since they rely on electronic DFT as well. However, these complex FPEC approaches strive to establish a potential reference self-consistently, which as yet cannot be achieved with sufficient accuracy. Not employing a fixed reference frame for the potential, the potential scale will experience an uncontrollable drift caused by electric field effects in the boundary region, which are structure sensitive and highly non-linear. If the FPEC approach does not adequately project the configuration of the boundary region, it will fail at reproducing the correct double layer properties. Recent works suggest that FPEC approaches capture the capacitive response of the interface

only close to the potential of zero charge and even there the agreement is qualitative at best [86].

Consistent treatment of the boundary region in Figure 3 transpires as the crucial challenge of computational approaches. Consequently, none of 265 the existing approaches reproduces the non-monotonic relation in Figure 2. 266 JDFT, which relies on the formulation of a free energy functional for the electrochemical interface, offers the best prospects for addressing this challenge. 268 The approach must be extended with functionals for the boundary region to account for specific surface states and local solvent polarization effects. The 270 theoretical framework discussed in the previous section should provide guidance in this regard. It suggests that (at least) two additional field-dependent variables must be considered in variational free energy minimization: a vari-273 able for the surface configuration of the catalyst and a variable for the order-274 ing of near-surface solvent molecules. These functionals could be determined 275 self-consistently, demanding dynamic or reactive versions of JDFT, or they must be parameterized empirically using experimental data.

# Acknowledgments

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## 285 Figure Captions

Figure 1: General schematic outline for theoretical-computational methodologies in electrocatalysis. The central challenge is to solve a self-consistency problem for pre-set electrode potential and electrolyte composition (represented symbolically by the pH). Other macroscopic operating parameters and external conditions must be controlled as well. The problem involves a non-linear coupling of phenomena in three regions, viz. electrode region, electrolyte region and a boundary region in-between.

Figure 2: "Free" metal surface charge density at a Pt electrode vs. electrode potential, as seen by ions in electrolyte solution. (a) shows surface excesses of sodium and sulfate ions as function of  $\phi^{\rm M}$ , obtained from radiotracer measurements. In the normal region on the left, cation concentration decreases with increasing  $\phi^{\rm M}$  in response to the decrease in electronic charge on the metal. Above the first potential of zero charge, at  $\approx 0.5$  V<sub>SHE</sub>, chemisorbed oxygen species form. An inverted charging region occurs for  $\phi^{\rm M} > 0.9$  V<sub>SHE</sub>, with a transition to negative excess "free" charge. Adapted with permission [37]. Copyright 1975, Elsevier. Part (b) shows the electrode charging relation calculated in the model of Huang et al. [73], which reproduces the nonlinear and non-monotonic trends in (a). Reprinted with permission [73]. Copyright 2016, American Chemical Society.

Figure 3: Schematic of the electrode-electrolyte interface, showing electrode region, electrolyte region and boundary region in-between. Simulation methodologies for different regions are indicated at the lower edge. Different flavours of first-principles approaches to study the electrochemical interface are indicated along the bottom rail.

Figure 4: Deciphering the oxygen reduction reaction [78]. A reaction mechanisms is identified and the reaction pathway is parameterized using basic KS-DFT calculations (bottom, left). Microkinetic modeling (bottom, centre) gives an expression for net reaction rate (equation in the centre). Separately, the electrochemical interface model can be solved (bottom, right), using the theory in Ref. [73], to obtain the metal charging relation. The fully parameterized approach provides as output mechanistic insights, e.g., rate-determining term in the net reaction rate; descriptor-based activity assessment for materials screening; and effective parameters like Tafel-slope or exchange current density to use in porous electrode models.

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